



# Carbon capture and utilisation technologies applied to energy conversion systems and other energy-intensive applications

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# Outline

1. Introduction
2. Carbon capture and utilisation technologies
3. Major design assumptions
4. Plant modelling, simulation and thermal integration
5. Evaluation of carbon capture and utilisation technologies for energy-intensive applications
6. Conclusions



# I. Introduction

The following work was performed within the project:  
***“Developing innovative low carbon solutions for energy-intensive industrial applications by Carbon Capture, Utilization and Storage (CCUS) technologies”***

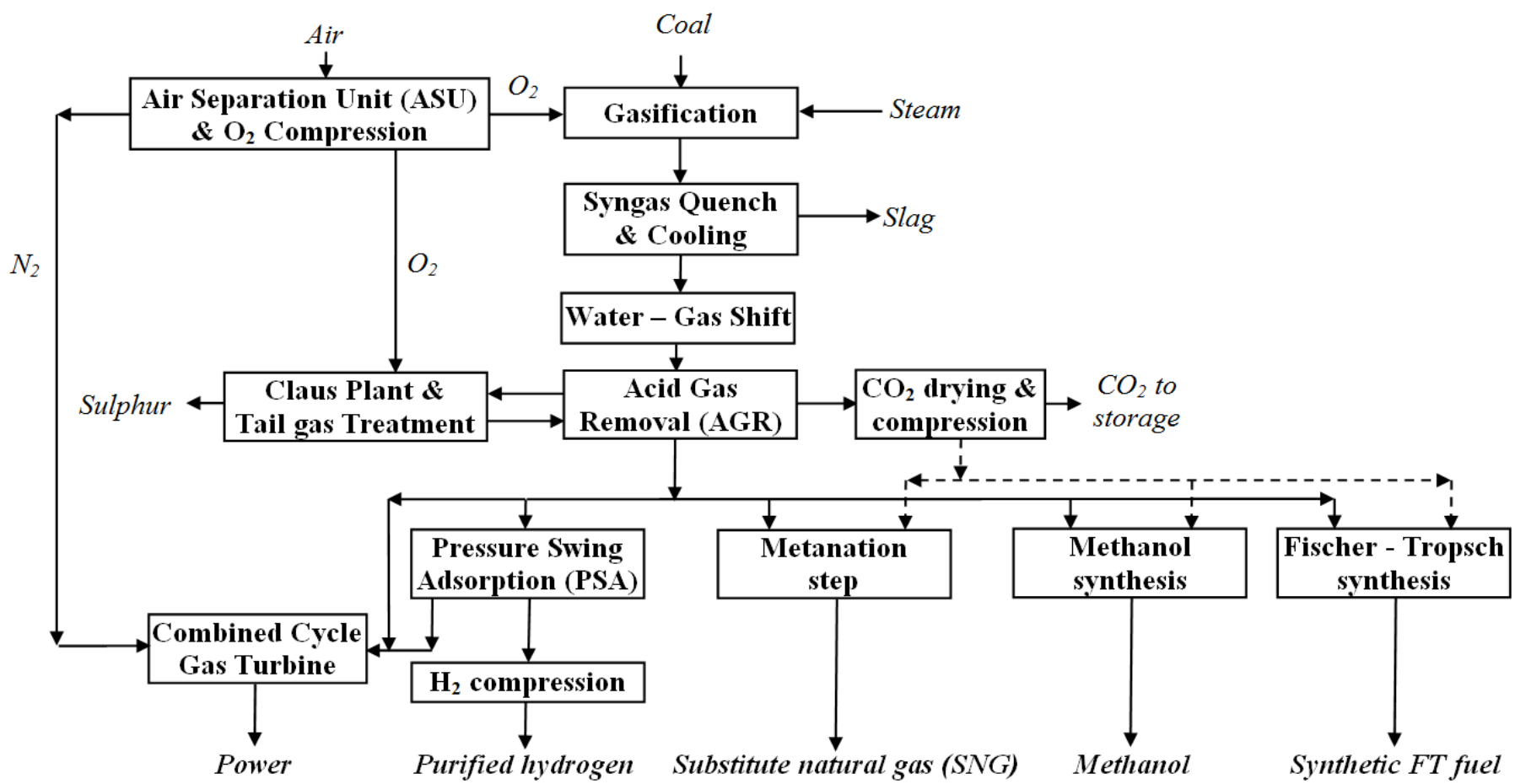
**Specific project objectives:**

- Investigation of fossil fuel-intensive industrial processes e.g. heat & power, metallurgy, cement, petro-chemistry
- Energy vectors poly-generation (power, H<sub>2</sub>, SNG, MeOH)
- Evaluation of various carbon capture and utilisation technologies e.g. reactive gas-liquid & gas-solid systems
- Techno-economical and environmental evaluations of energy-intensive industrial applications with CCUS



# Energy vector poly-generation concepts based on gasification process with CO<sub>2</sub> capture

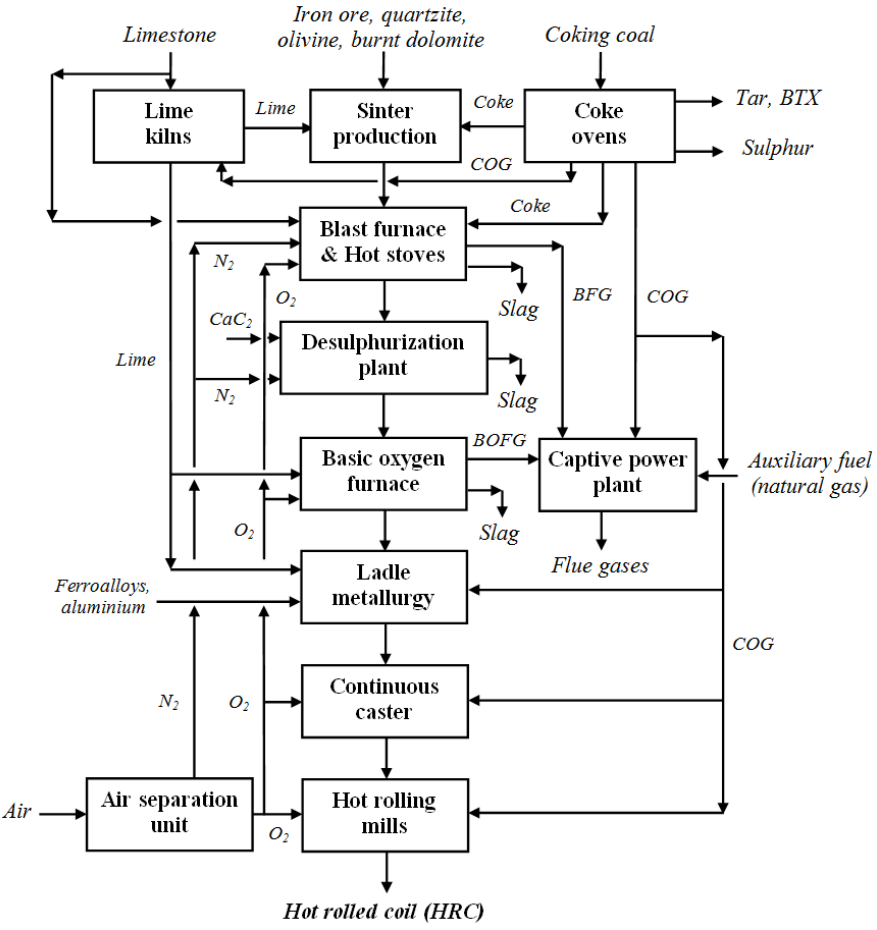
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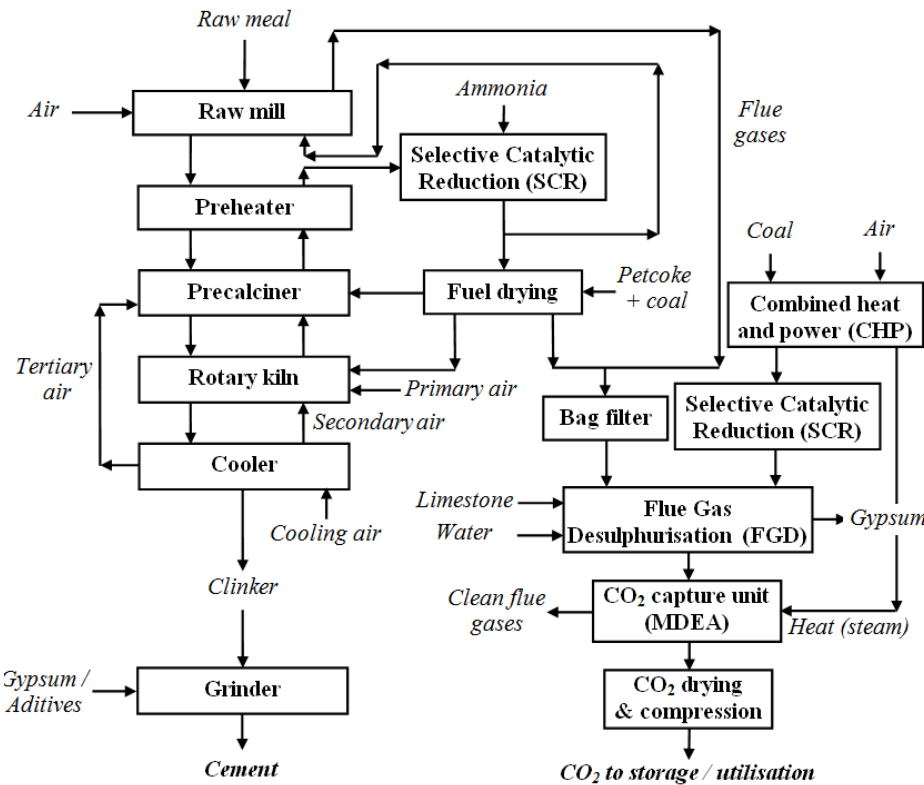


# Decarbonisation of energy-intensive industrial processes (non-power applications)

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**Integrated steel mill**

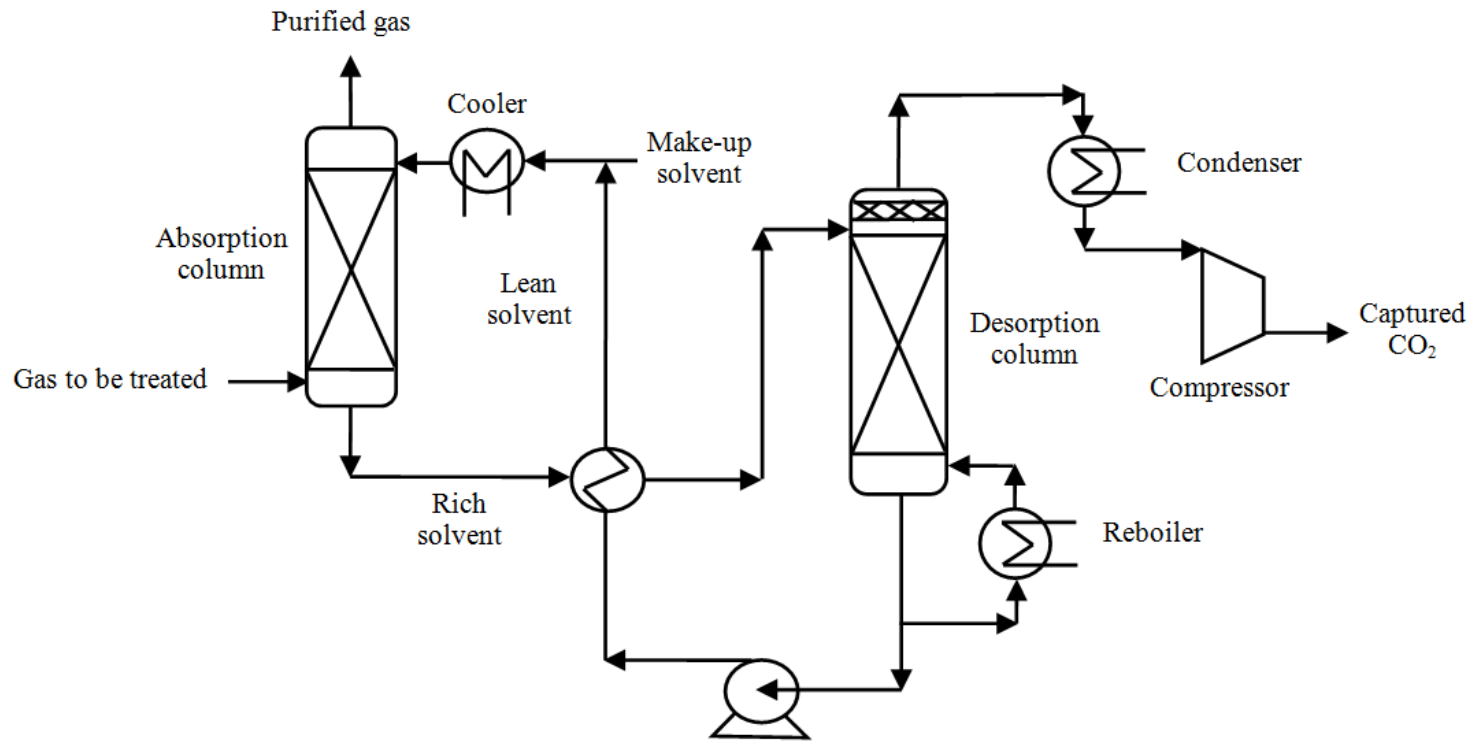
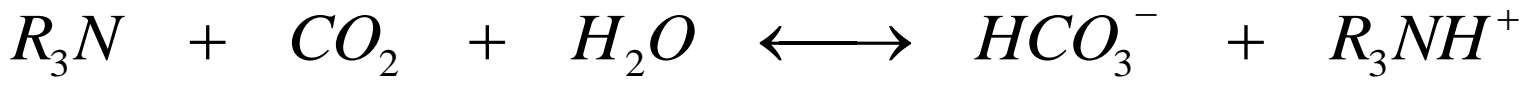


**Cement production plant**

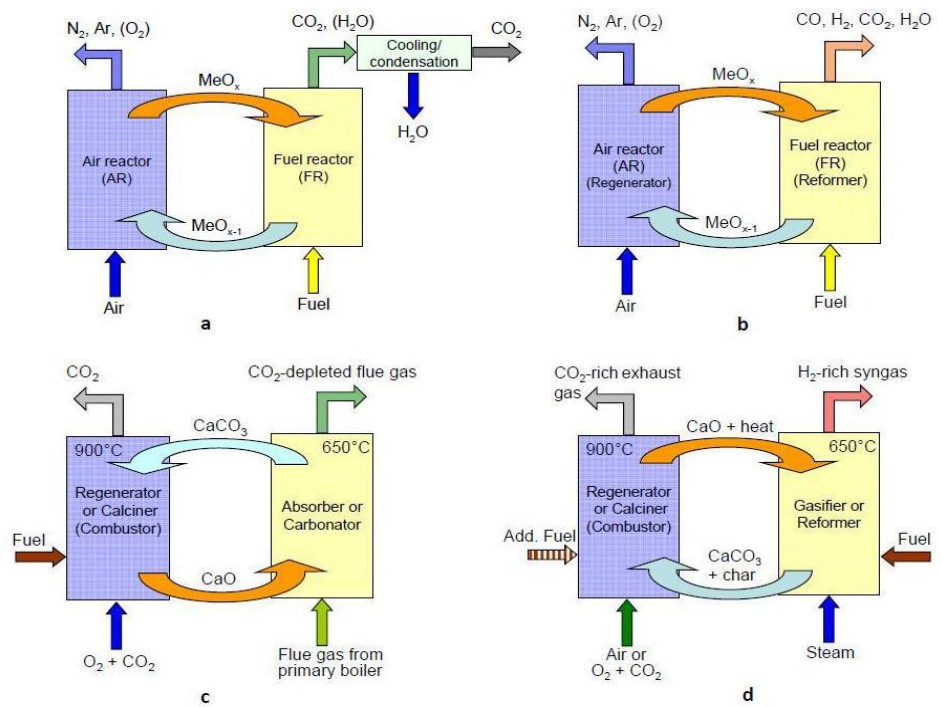
# II. Carbon capture and utilisation

## CO<sub>2</sub> capture based on gas-liquid absorption

Chemical reactions for tertiary alkanolamine (e.g. MDEA):



# CO<sub>2</sub> capture based on chemical & calcium looping systems



	Technology	Transported reactive species	Circulating solid material	Obtained product
a	Chemical looping combustion (CLC)	O <sub>2</sub>	metal oxides	heat, power, CO <sub>2</sub>
b	Chemical looping reforming (CLR)	O <sub>2</sub>	metal oxides	H <sub>2</sub> , CO
c	Carbonate Looping	CO <sub>2</sub>	CaO/ CaCO <sub>3</sub>	clean flue gas, CO <sub>2</sub>
d	Sorption enhanced reforming (SER)	CO <sub>2</sub>	CaO/ CaCO <sub>3</sub>	hydrogen rich syngas

## Main advantages:

- Inherent CO<sub>2</sub> capture
- High temperature heat recovery potential
- Fuel versatility
- Poly-generation capability

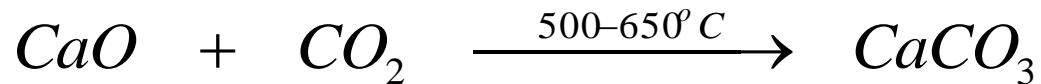




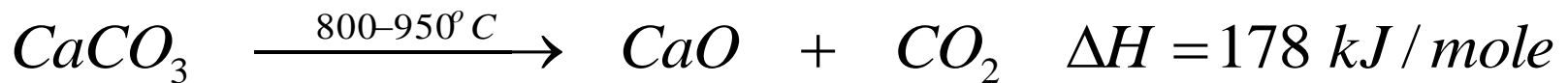
# CO<sub>2</sub> capture based on calcium looping (CaL)

## Chemical reactions for post-combustion capture:

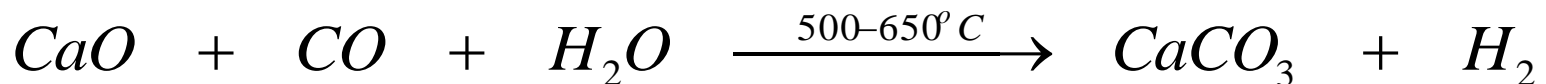
- Carbonation reactor:



- Calcination reactor (required extra heat input):



**A distinct design option for pre-combustion CO<sub>2</sub> capture is Sorbent Enhanced Water Gas Shift (SEWGS):**

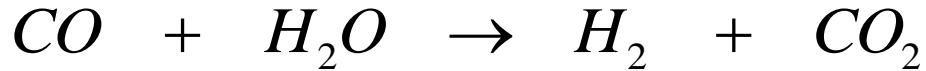




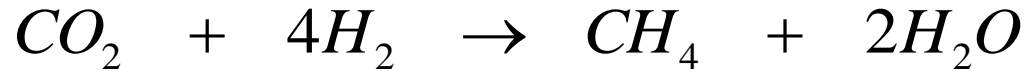
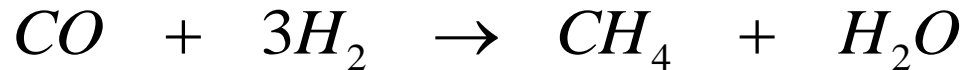


# Energy vectors poly-generation

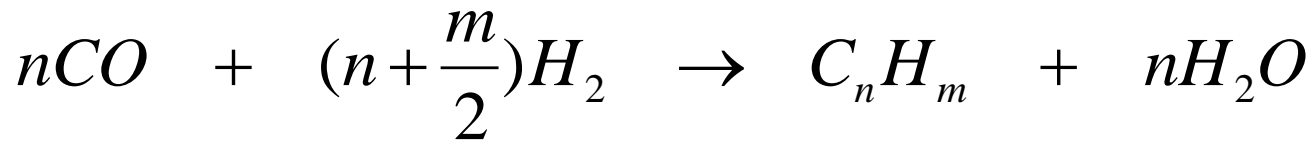
- **Hydrogen production (water gas shift - WGS):**



- **Substitute natural gas (SNG) production:**



- **Liquid hydrocarbons production (FT fuel):**



- **Methanol and Di-Methyl Ether (DME) production:**



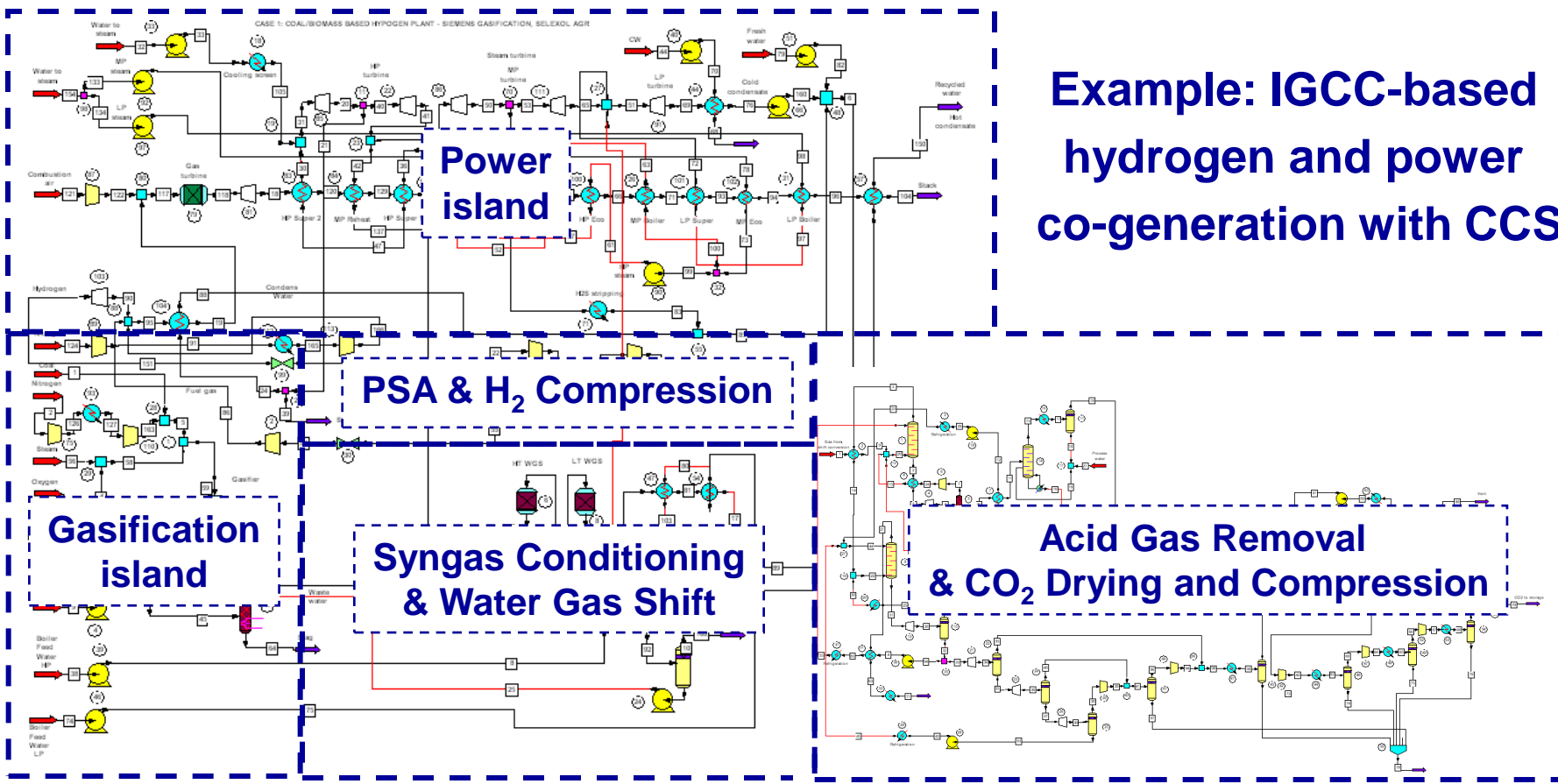
## III. Major design assumptions

1. **Power plants: Integrated gasification combined cycle / Super-critical pulverised coal (400 - 600 MW<sub>e</sub> net)**
2. **Other industrial applications: Integrated steel mill (4 Mt/y), cement production plant (1 Mt/y)**
3. **Carbon capture rate: 90%**
4. **CO<sub>2</sub> capture (pre- & post-combustion): MDEA / CaL**
5. **CO<sub>2</sub> purity & pressure: >95% (vol.) / 120 bar**
6. **Other energy carriers: H<sub>2</sub>, SNG, Methanol, FT fuel**
7. **Fuel: Coal, natural gas (auxiliary fuel for steel mill)**

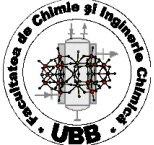
# IV. Plant modeling, simulation and thermal integration

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Investigated case studies were simulated using process flow modelling (ChemCAD software)

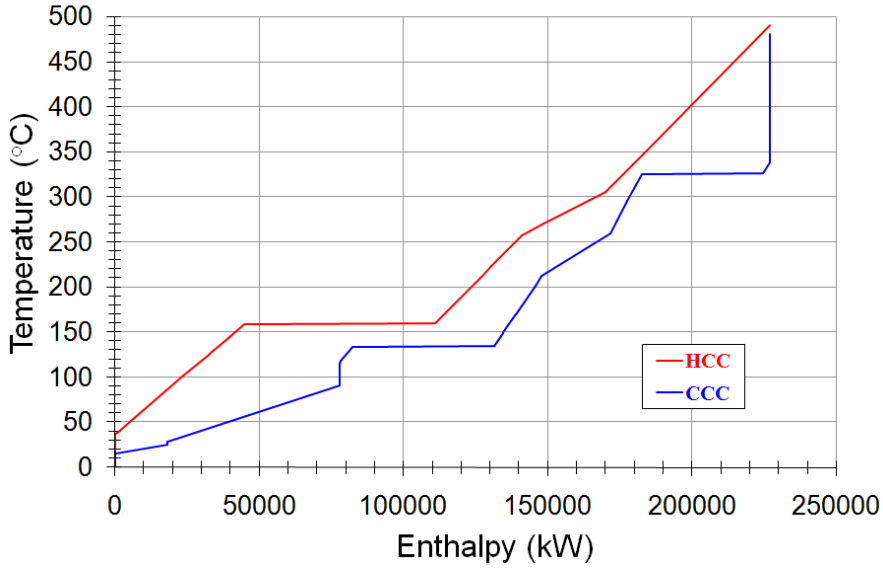


Example: IGCC-based hydrogen and power co-generation with CCS



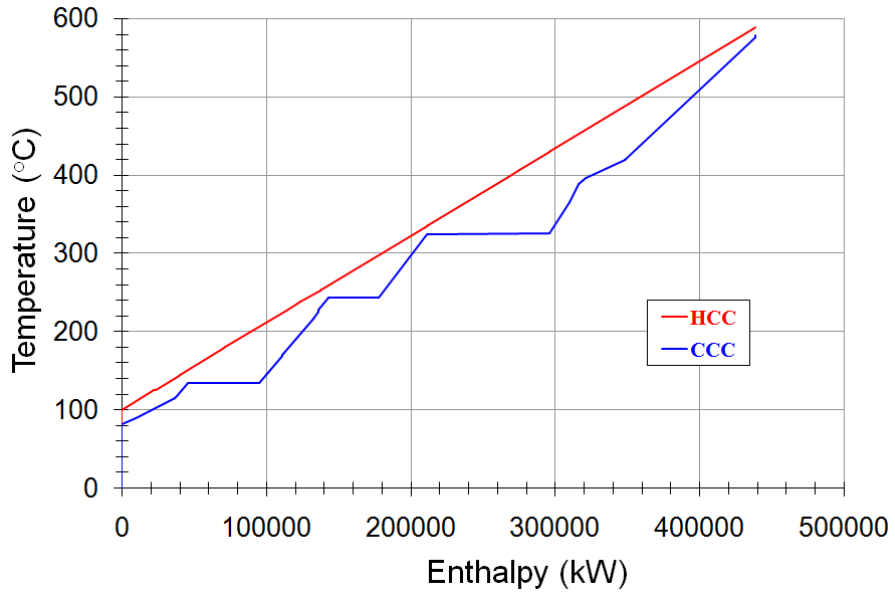
# Optimization of plant energy efficiency by heat and power integration

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Composite curves for syngas treatment line

## Example: IGCC-based hydrogen and power co-generation with CCS



Composite curves for hydrogen-fuelled CCGT



# V. Evaluation of CCUS technologies for energy-intensive industrial applications

Investigated energy-intensive industrial applications:

## *(i) IGCC power plants (dry feed gas quench gasifier)*

- Case 1a – Plant without carbon capture (benchmark)
- Case 1b – Post-combustion CO<sub>2</sub> capture (MDEA)
- Case 1c – Pre-combustion CO<sub>2</sub> capture (MDEA)
- Case 1d – Post-combustion CO<sub>2</sub> capture (CaL)
- Case 1e – Pre-combustion CO<sub>2</sub> capture (CaL)

## *(ii) Super-critical PC power plants*

- Case 2a – Plant without carbon capture (benchmark)
- Case 2b – Post-combustion CO<sub>2</sub> capture (MDEA)
- Case 2c – Post-combustion CO<sub>2</sub> capture (CaL)



## Investigated energy-intensive industrial applications:

### *(iii) Integrated steel mills*

**Case 3a – Plant without carbon capture (benchmark)**

**Case 3b – Post-combustion CO<sub>2</sub> capture (MDEA) – A\***

**Case 3c – Post-combustion CO<sub>2</sub> capture (MDEA) – B\*\***

**Case 3d – Post-combustion CO<sub>2</sub> capture (CaL) – A\***

**Case 3e – Post-combustion CO<sub>2</sub> capture (CaL) – B\*\***

\*A – CO<sub>2</sub> capture from hot stoves & steam / power plant

\*\*B – CO<sub>2</sub> capture from hot stoves, steam / power plant, lime kilns & coke ovens

### *(iv) Cement production plants*

**Case 4a – Plant without carbon capture (benchmark)**

**Case 4b – Post-combustion CO<sub>2</sub> capture (MDEA)**

**Case 4c – Post-combustion CO<sub>2</sub> capture (CaL)**



# IGCC power plants



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		Case 1a	Case 1b	Case 1c	Case 1d	Case 1e
Coal flowrate	t/h	150.50	150.50	166.91	228.14	221.88
Coal thermal energy	MW <sub>th</sub>	1052.25	1052.25	1166.98	1595.12	1551.35
Gas turbine output	MW <sub>e</sub>	334.00	334.00	334.00	334.00	334.00
Steam turbine output	MW <sub>e</sub>	225.30	139.56	200.72	384.60	380.71
Expander output	MW <sub>e</sub>	1.42	1.42	1.18	1.78	1.42
Ancillary power	MW <sub>e</sub>	76.11	95.86	108.82	176.41	156.05
Net power	MW <sub>e</sub>	484.61	379.12	427.08	547.97	560.08
Net power efficiency	%	46.05	36.03	36.59	34.35	36.10
Carbon capture rate	%	0.00	90.00	90.00	90.00	90.00
CO <sub>2</sub> emissions	kg / MWh	759.57	92.15	85.51	99.82	82.83
SPECCA	MJ / kg	-	3.25	2.99	4.03	3.18





# Super-critical PC power plants



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		Case 2a	Case 2b	Case 2c
Coal flowrate	t/h	156.74	198.35	216.74
Coal thermal energy	MW <sub>th</sub>	1095.87	1386.79	1515.37
Steam turbine output	MW <sub>e</sub>	502.32	541.30	649.60
Ancillary power	MW <sub>e</sub>	27.45	65.68	105.38
Net power	MW <sub>e</sub>	474.87	475.62	544.22
Net power efficiency	%	43.33	34.29	35.91
Carbon capture rate	%	0.00	90.00	90.00
CO <sub>2</sub> emissions	kg / MWh	800.58	89.55	76.84
SPECCA *	MJ / kg	-	3.07	2.37

\* SPECCA - Specific primary energy consumption for CO<sub>2</sub> avoided =  $\frac{\text{Heat rate}_{\text{CO}_2 \text{ capture}} - \text{Heat rate}_{\text{no capture}}}{\text{Emissions}_{\text{CO}_2 \text{ no capture}} - \text{Emissions}_{\text{CO}_2 \text{ capture}}}$

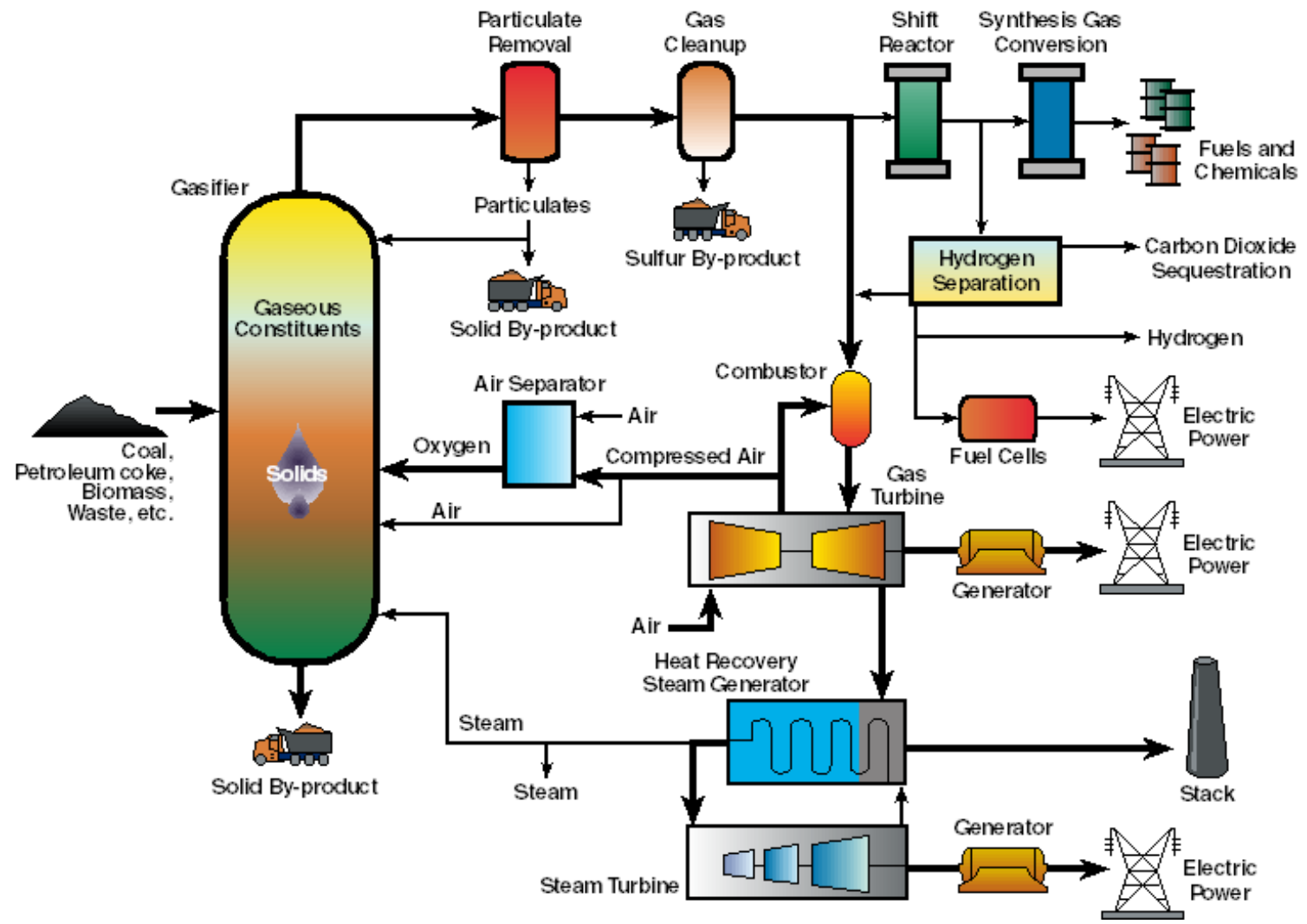
# Integrated steel mills

		Case 3a	Case 3b	Case 3c	Case 3d	Case 3e
Fuel thermal energy	$MW_{th}$	669.78	517.25	544.00	882.04	1156.79
Gas turbine output	$MW_e$	-	192.00	202.31	91.06	91.06
Steam turbine output	$MW_e$	224.68	101.76	107.33	269.64	366.04
Ancillary power	$MW_e$	9.68	1.59	1.64	76.04	132.57
Net power	$MW_e$	215.00	292.17	308.00	284.66	324.53
Net power efficiency	%	32.10	56.48	56.61	32.27	27.79
CO <sub>2</sub> emissions power	kg / MWh	2455.33	370.60	369.67	152.39	242.40
Carbon capture rate	%	0.00	90.00	90.00	90.00	90.00
CO <sub>2</sub> emissions steel	kg / tHRC	2092.45	1048.36	833.54	1203.61	640.01
Captured CO <sub>2</sub>	kg / tHRC	0.00	1300.88	1615.81	824.45	1495.12

# Cement production plants

		Case 4a	Case 4b	Case 4c
Coal flowrate	t/h	-	33.47	22.00
Coal thermal energy	MW <sub>th</sub>	-	234.06	153.81
Steam turbine output	MW <sub>e</sub>	-	54.42	58.01
Ancillary power	MW <sub>e</sub>	16.24	34.14	42.19
Net power	MW <sub>e</sub>	-	20.28	15.82
Net power efficiency	%	-	8.66	10.28
Carbon capture rate	%	0.00	90.00	90.00
CO <sub>2</sub> emissions	kg / t cement	770.44	55.83	58.37
Captured CO <sub>2</sub>	kg / t cement	0.00	1214.15	962.19

# Gasification-based energy vector poly-generation system with CO<sub>2</sub> capture





# Various energy vectors and power co-generation based on gasification (Case 1c)

		SNG	Methanol	FT fuel
Coal thermal energy	MW <sub>th</sub>	1224.51	298.02	1224.51
Gross power output	MW <sub>e</sub>	164.75	40.12	193.25
SNG thermal output	MW <sub>th</sub>	800.00	-	-
Methanol thermal output	MW <sub>th</sub>	-	150.00	-
FT fuel thermal output	MW <sub>th</sub>	-	-	700.00
Ancillary power demand	MW <sub>e</sub>	116.23	22.56	76.45
Net power output	MW <sub>e</sub>	48.52	17.56	116.80
Net electrical efficiency	%	3.96	5.89	9.53
SNG / MeOH / FT efficiency	%	65.33	50.33	57.16
Cumulative efficiency	%	69.28	56.22	66.70
Carbon capture rate	%	60.00	50.00	48.00
CO <sub>2</sub> specific emissions	kg / MWh	8.25	24.32	37.45

## VI. Conclusions

- Various energy-intensive industrial applications (power generation, integrated steel mill, cement production) were evaluated in view of decarbonisation
- Modelling, simulation and heat & power integration tools were used to assess and optimize the plant performances
- Calcium looping method looks very promising to deliver high energy efficiency in comparison to the reactive gas-liquid absorption for energy-intensive applications
- Energy vectors poly-generation concepts are promising to further improve the technical and environmental performances (e.g. overall energy efficiency, specific CO<sub>2</sub> emissions, plant flexibility etc.)



# Thank you for your attention!

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